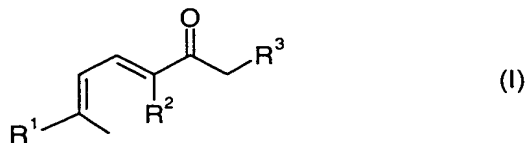
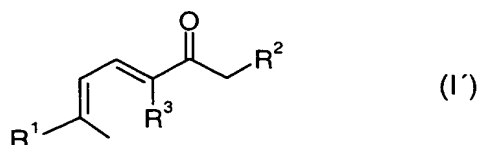


What is claimed is:

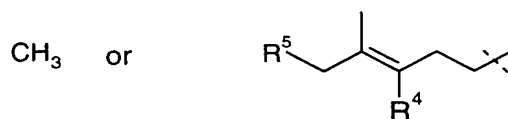
1. A continuous process for preparing pseudoionones of the general formulae I or I' and isomers thereof



or



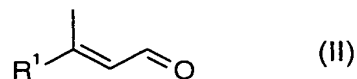
where R<sup>1</sup> is



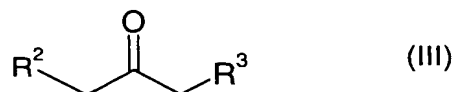
R<sup>2</sup>, R<sup>3</sup> are each hydrogen, CH<sub>3</sub> or C<sub>2</sub>H<sub>5</sub>,

R<sup>4</sup>, R<sup>5</sup> are each hydrogen or CH<sub>3</sub>,

by reacting an aldehyde of the formula (II)



with an excess of a ketone of the general formula (III)



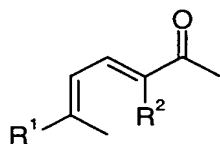
where R<sup>1</sup>, R<sup>2</sup> and R<sup>3</sup> are each as defined above, in the presence of water and alkali metal hydroxide at elevated temperature in homogeneous solution, which comprises

## 12

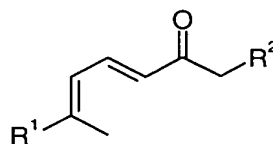
- 5
- a) mixing the homogeneous solution of aldehyde, ketone and aqueous alkali metal hydroxide at a temperature of from 10 to 120°C, then
- b) removing the water and alkali metal hydroxide which have not dissolved in the reaction mixture,
- 10
- c) subsequently passing the homogeneous reaction mixture, avoiding backmixing, at a temperature which is from 10 to 120°C above the boiling point of the lowest-boiling component and a vapor pressure  $p$  of from  $10^6$  to  $10^7$  Pa through a reactor which enables a residence time of from 2 to 300 minutes,
- d) cooling the reaction mixture under decompression,
- 15
- e) removing the ketone from the reaction mixture with steam in countercurrent and
- f) drying the crude product and freeing it of excess aldehyde and secondary components using a rectification column.
- 20
2. The process according to claim 1, wherein the ketone component of the general formula (II) is added in a from 5- to 50-fold molar excess, and the unconverted proportion, downstream of the reaction zone, is removed at a pressure of from  $10^7$  to  $5 \cdot 10^8$  mPa<sub>abs.</sub> and added again to the fresh ketone for the synthesis.
- 25
3. The process according to claim 1 or 2, wherein the reaction temperature at a given residence time is selected in such a way that the conversion of the aldehyde component is from 60 to 98%, and the unconverted aldehyde is removed and recycled into the reaction.
- 30
4. The process according to claims 1 to 3, wherein the water content of the ketone, used for the reaction, of the formula (III) is between 1 and 15% by weight.
- 35
5. The process according to claims 1 to 4, wherein the concentration of the alkali metal hydroxide used for the reaction is between 0.005 and 50% by weight, preferably 5 – 10% by weight.
6. The process according to claims 1 to 5 for preparing pseudoionones of the formula I and isomers thereof where  $R^2$  or  $R^3$  is methyl, wherein the concentration of the alkali metal

hydroxide used for the reaction is from 10 to 50% by weight, preferably from 35 to 45% by weight.

7. The process according to claims 1 to 6, wherein the ketone of the formula (III) used consists substantially of excess ketone of the formula (III) which has been removed from the reaction and has a water content of 1 – 15% by weight, which may be supplemented with either anhydrous or aqueous ketone of the formula (III) having a water content of 1 – 15% by weight.
- 10 8. The process according to claims 1 to 7, wherein, in the case of reaction with ketones of the general formula (III) where  $R^2 \neq H$  and  $R^3 = H$ , a product mixture is obtained which contains from 70 to 95% n-alkylpseudoionones and from 5 to 30% isoalkylpseudoionones

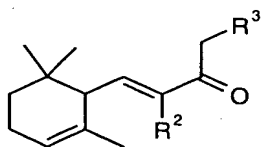


iso - alkylpseudoionone

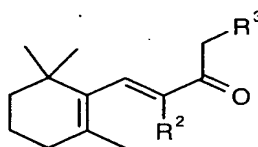


n - alkylpseudoionone

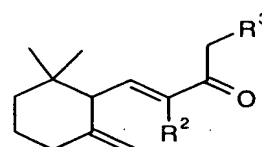
- 15 9. A continuous process for preparing ionones of the general formulae (IV), (V) and (VI) and isomers thereof, which comprises reacting the pseudoionones obtained according to claims 1 to 8 to give ionones of the general formulae (IV) to (VI)



$\alpha$ -Isomer  
(IV)



$\beta$ -Isomer  
(V)



$\gamma$ -Isomer  
(VI)

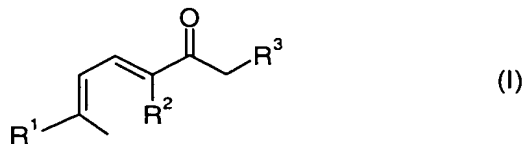
in the form such that the ratio of the n-form ( $R^2 = H$ ,  $R^3 = \text{alkyl}$ ) to the iso-form ( $R^2 = \text{alkyl}$ ,  $R^3 = H$ ) according to claim 8 is maintained.

- 25 10. The process according to claim 9, wherein the pseudoionones obtained according to claims 1 to 8 are reacted with highly concentrated sulfuric acid in the presence of a diluent which is inert under the reaction conditions to give ionones, the reaction temperature being 0-20°C and the residence time between cyclization and hydrolysis being from 10 to 300 seconds, preferably 120 seconds.

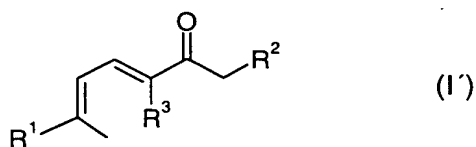
Continuous preparation of pseudoionones and ionones

Abstract

- 5 A continuous process for preparing pseudoionones of the general formulae I or I' and isomers thereof

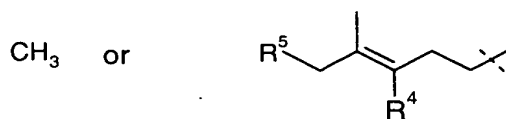


or



10

where R¹ is

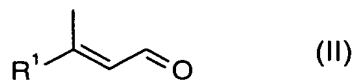


- 15 R², R³ are each hydrogen, CH<sub>3</sub> or C<sub>2</sub>H<sub>5</sub>,

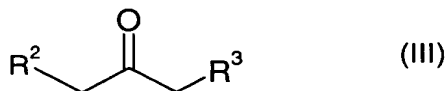
R⁴, R⁵ are each hydrogen or CH<sub>3</sub>,

by reacting an aldehyde of the formula (II)

20



with an excess of a ketone of the general formula (III)



25

where R¹, R² and R³ are each as defined above, in the presence of water and alkali metal hydroxide at elevated temperature in homogeneous solution, which comprises

- a) mixing the homogeneous solution of aldehyde, ketone and aqueous alkali metal hydroxide at a temperature of from 10 to 120°C, then
- 5 b) removing the water and alkali metal hydroxide which have not dissolved in the reaction mixture,
- c) subsequently passing the homogeneous reaction mixture, avoiding backmixing, at a temperature which is from 10 to 120°C above the boiling point of the lowest-boiling  
10 component and a vapor pressure  $p$  of from  $10^6$  to  $10^7$  Pa through a reactor which enables a residence time of from 2 to 300 minutes,
- d) cooling the reaction mixture under decompression,
- 15 e) removing the ketone from the reaction mixture with steam in countercurrent and
- f) drying the crude product and freeing it of excess aldehyde and secondary components using a rectification column.